

# Simutech Project

# IIT Kanpur



## Distillation Column Design

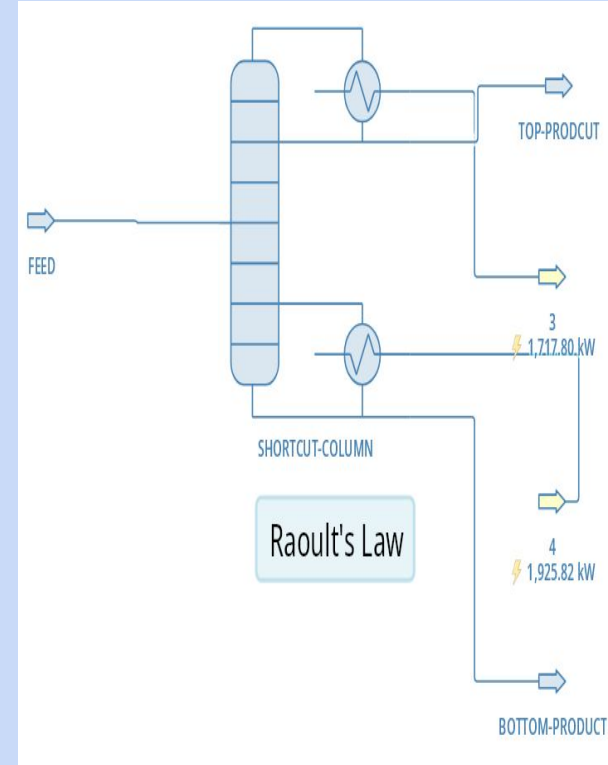
**Mentors:**

**Samanvay Lakhotia & Raju Singh**

End-Term Report :  
**SAREN AJMERA & SUSHMITA**

# Project Objectives

- Using Python/MATLAB, optimise a Continuous Distillation Column for a binary mixture.
- Outline a binary distillation column in Python/MATLAB, utilise the McCabe Thiele process to investigate the column, and derive conclusions from the process.
- Understand Azeotropic mixtures.
- Automate the Inspection pipelines to determine the minimal and real number of stages required to accomplish the desired separation, as well as the Minimum Reflux Ratio, utilising Graph-based Visualisations.
- Simulating the construction of a distillation column using simulation tools such as DWSIM or Aspen.

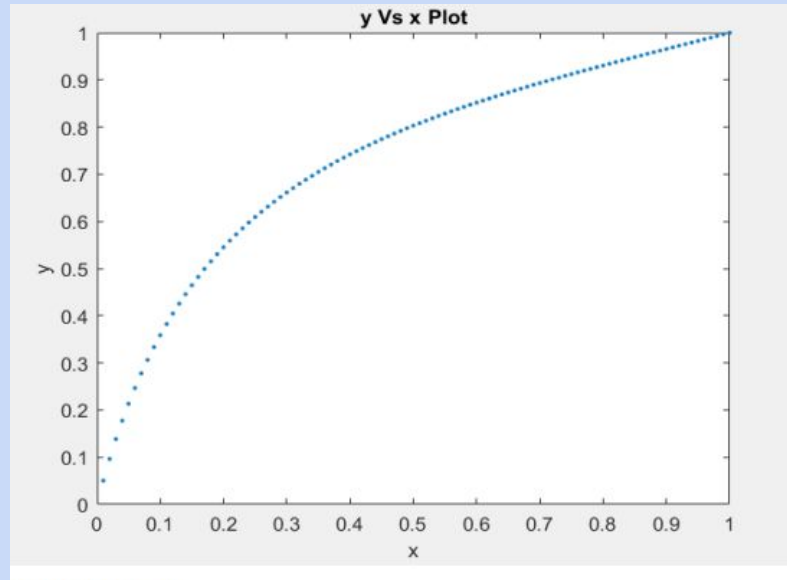


- Learning different distillation techniques.
  - 1.Extractive Distillation
  - 2.Azeotropic Distillation
  - 3.Pressure Swing Distillation

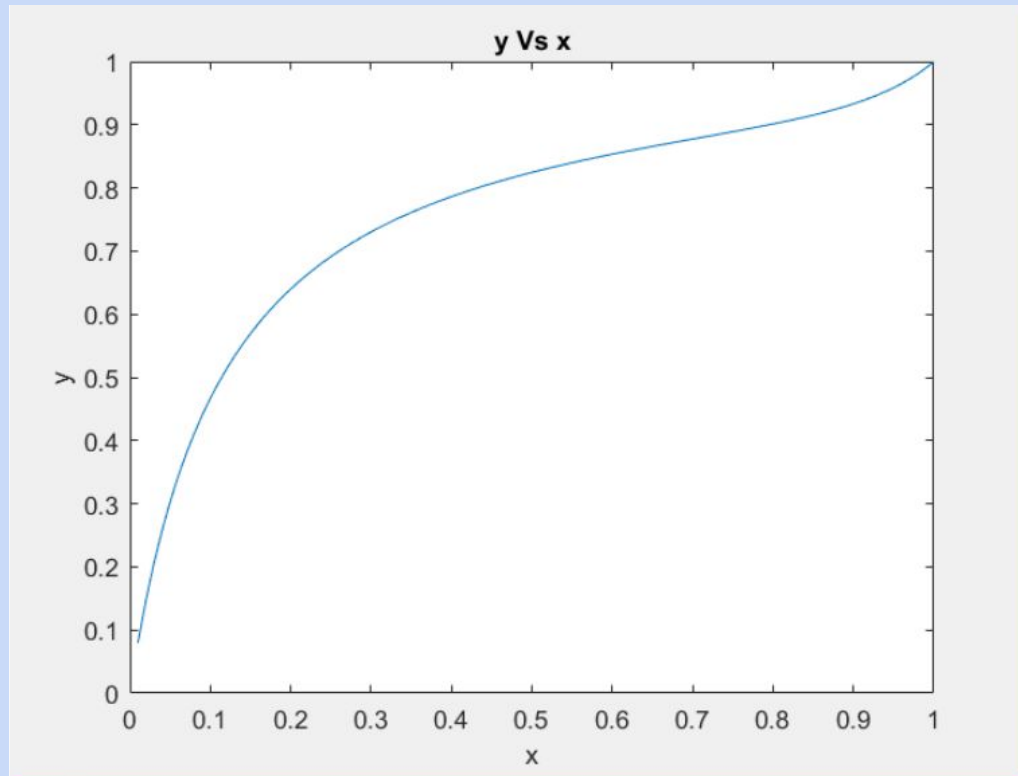
As part of this project on the design of distillation columns, we were tasked with completing three separate assignments.

# ASSIGNMENT 1

Assignment 1 focused mostly on studying the fundamentals of Raoult's law and various activity coefficient models. Using MATLAB code to implement Raoult's Law and one activity coefficient model for the binary azeotropic system.



y Vs x Plot Using Raoult's Law



**y Vs x plot using Van Laar Coefficient Model**

# ASSIGNMENT 2

In this assignment, we computed

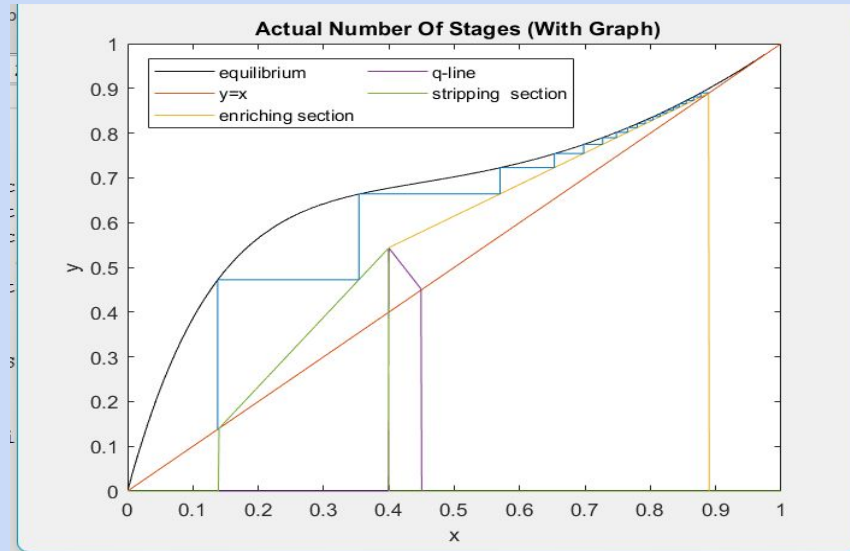
1. ACTUAL NUMBER OF STAGES
2. MINIMUM NUMBER OF STAGES
3. MINIMUM REFLUX RATIO

in a distillation column for

1. Non-ideal solution (using Van Laar's Method)
2. Ideal solution

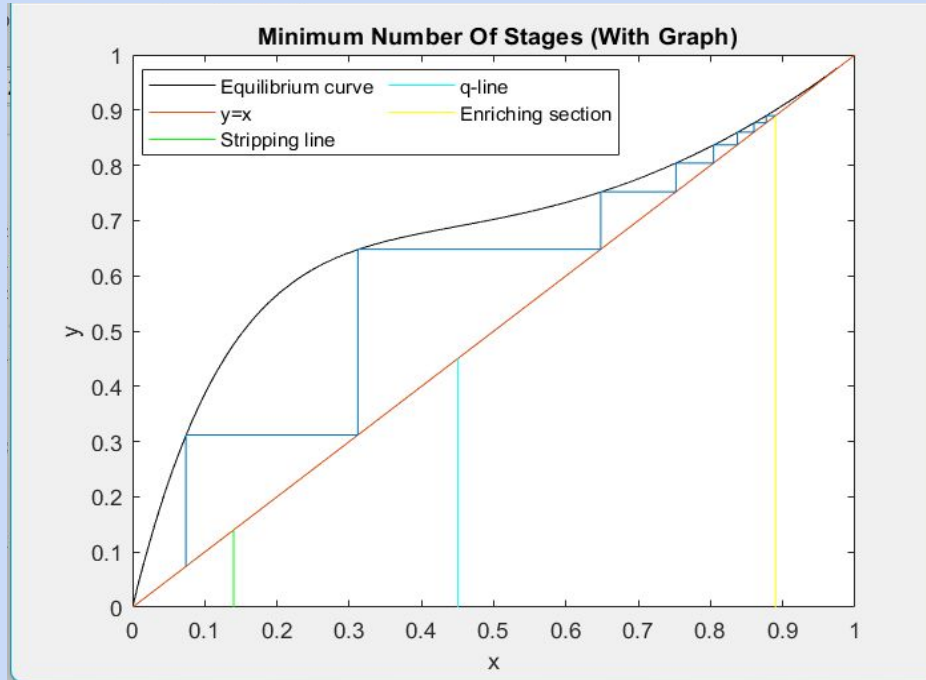
Here we have listed the respective methods of how we computed the above mentioned quantities :

1. We calculated ACTUAL NUMBER OF STAGES by first finding the point where q-line, enriching section line and stripping section line intersects and then constructed the triangles to commute the actual number of stages.



Calculating actual number of stages in non-ideal case

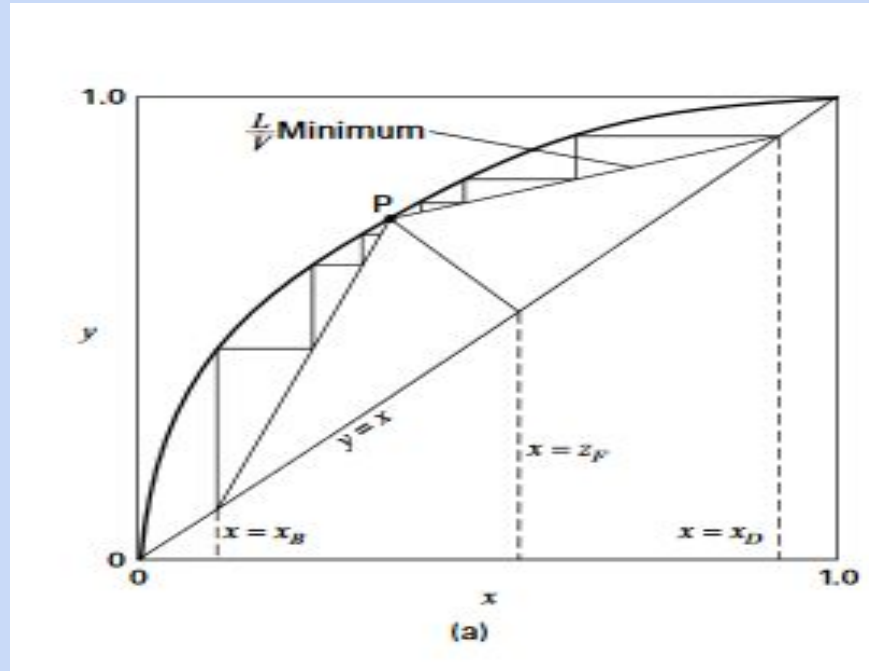
2. To calculate MINIMUM NUMBER OF STAGES, the point of intersection of above three lines comes on  $y=x$  line and thus constructing the triangles gives us the minimum number of stages.



Calculating minimum number of stages

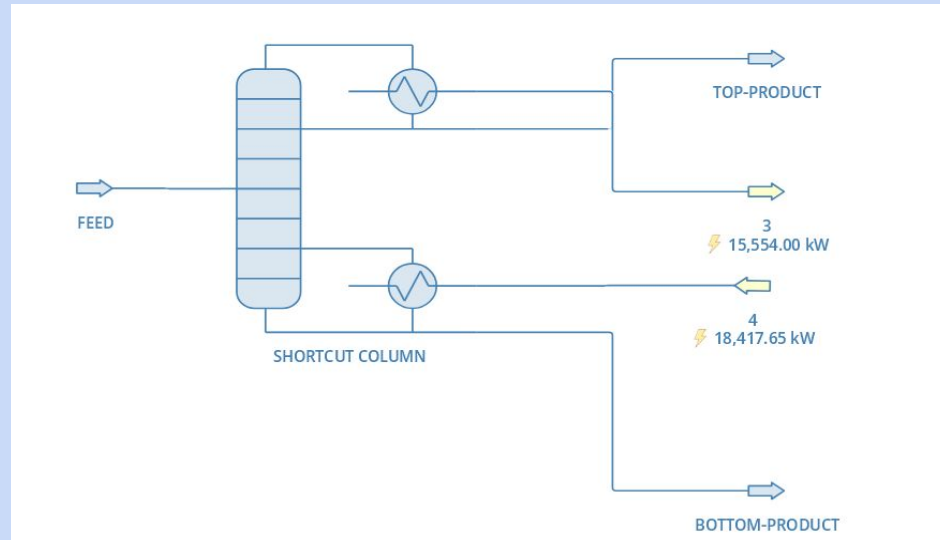


3. To calculate MINIMUM REFLUX RATIO, we first calculated point of intersection of q-line and equilibrium curve. Then we extrapolated the enriching section line from this point to intersect on the y-axis. We used this y-intercept to calculate the minimum reflux ratio.



# ASSIGNMENT 3

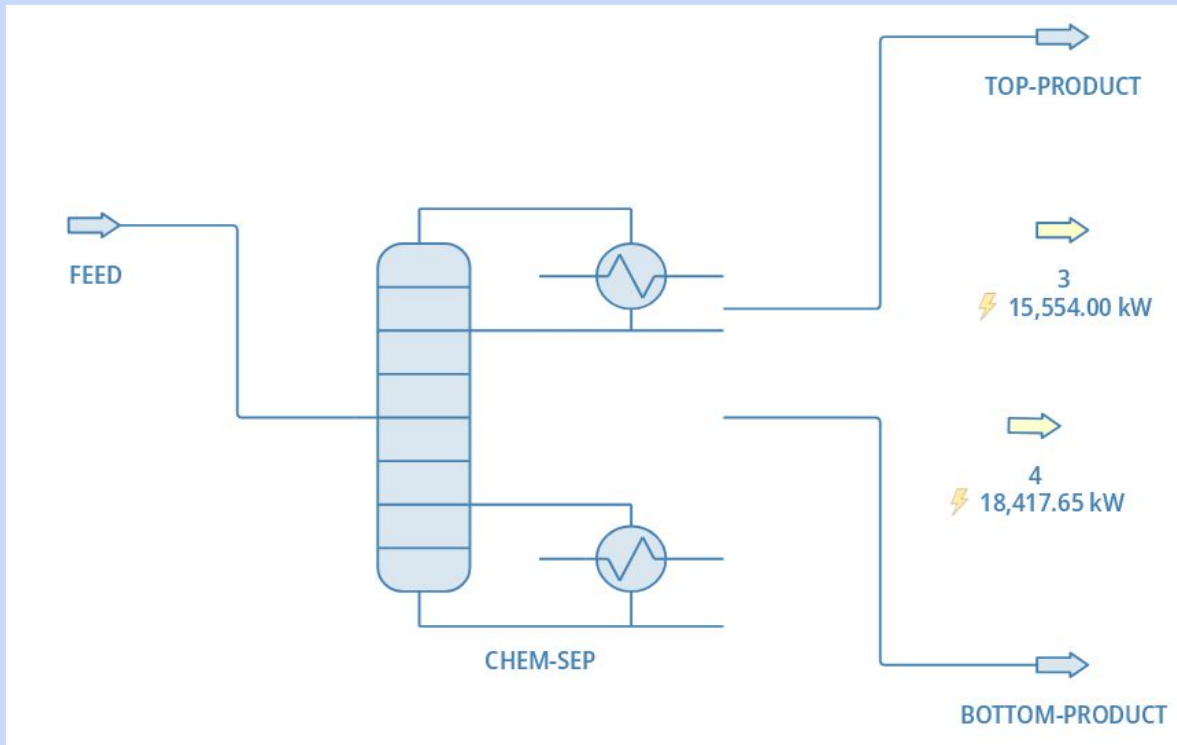
In this assignment we firstly simulated a distillation column & verified the results of the Python/MATLAB code through the DWSIM software for the system of ethanol and water.



Flow Sheet using Shortcut column

By performing the simulations on DWSIM software using Shortcut Column , the results matched with MATLAB code results which proves the accuracy of the code and method for both ideal and non-ideal solution.

| DWSIM RESULTS  | MATLAB CODE RESULTS |       |  |          |       |       |                      |         |  |                          |         |  |                         |        |  |                    |         |  |                  |         |       |                |         |       |                 |         |       |               |         |       |                |       |    |               |         |    |  |
|--|---------------------|-------|--|----------|-------|-------|----------------------|---------|--|--------------------------|---------|--|-------------------------|--------|--|--------------------|---------|--|------------------|---------|-------|----------------|---------|-------|-----------------|---------|-------|---------------|---------|-------|----------------|-------|----|---------------|---------|----|--|
| <table border="1" data-bbox="193 516 823 945"><thead><tr><th colspan="3">Results</th></tr><tr><th>Property</th><th>Value</th><th>Units</th></tr></thead><tbody><tr><td>Minimum Reflux Ratio</td><td>1.93179</td><td></td></tr><tr><td>Minimum Number of Stages</td><td>9.22109</td><td></td></tr><tr><td>Actual Number of Stages</td><td>19.699</td><td></td></tr><tr><td>Optimal Feed Stage</td><td>5.57856</td><td></td></tr><tr><td>Stripping Liquid</td><td>560.135</td><td>mol/s</td></tr><tr><td>Rectify Liquid</td><td>282.357</td><td>mol/s</td></tr><tr><td>Stripping Vapor</td><td>400.015</td><td>mol/s</td></tr><tr><td>Rectify Vapor</td><td>400.006</td><td>mol/s</td></tr><tr><td>Condenser Duty</td><td>15554</td><td>kW</td></tr><tr><td>Reboiler Duty</td><td>18417.6</td><td>kW</td></tr></tbody></table> | Results             |       |  | Property | Value | Units | Minimum Reflux Ratio | 1.93179 |  | Minimum Number of Stages | 9.22109 |  | Actual Number of Stages | 19.699 |  | Optimal Feed Stage | 5.57856 |  | Stripping Liquid | 560.135 | mol/s | Rectify Liquid | 282.357 | mol/s | Stripping Vapor | 400.015 | mol/s | Rectify Vapor | 400.006 | mol/s | Condenser Duty | 15554 | kW | Reboiler Duty | 18417.6 | kW | <pre data-bbox="884 516 1647 915">Actual Number Of Stages(Trays) :<br/>18<br/><br/>Minimum Number Of Stages(Trays) :<br/>8<br/><br/>Minimum Reflux Ratio :<br/>1.974</pre> |
| Results  |                     |       |  |          |       |       |                      |         |  |                          |         |  |                         |        |  |                    |         |  |                  |         |       |                |         |       |                 |         |       |               |         |       |                |       |    |               |         |    |  |
| Property   | Value               | Units |  |          |       |       |                      |         |  |                          |         |  |                         |        |  |                    |         |  |                  |         |       |                |         |       |                 |         |       |               |         |       |                |       |    |               |         |    |  |
| Minimum Reflux Ratio   | 1.93179             |       |  |          |       |       |                      |         |  |                          |         |  |                         |        |  |                    |         |  |                  |         |       |                |         |       |                 |         |       |               |         |       |                |       |    |               |         |    |  |
| Minimum Number of Stages   | 9.22109             |       |  |          |       |       |                      |         |  |                          |         |  |                         |        |  |                    |         |  |                  |         |       |                |         |       |                 |         |       |               |         |       |                |       |    |               |         |    |  |
| Actual Number of Stages  | 19.699              |       |  |          |       |       |                      |         |  |                          |         |  |                         |        |  |                    |         |  |                  |         |       |                |         |       |                 |         |       |               |         |       |                |       |    |               |         |    |  |
| Optimal Feed Stage   | 5.57856             |       |  |          |       |       |                      |         |  |                          |         |  |                         |        |  |                    |         |  |                  |         |       |                |         |       |                 |         |       |               |         |       |                |       |    |               |         |    |  |
| Stripping Liquid   | 560.135             | mol/s |  |          |       |       |                      |         |  |                          |         |  |                         |        |  |                    |         |  |                  |         |       |                |         |       |                 |         |       |               |         |       |                |       |    |               |         |    |  |
| Rectify Liquid   | 282.357             | mol/s |  |          |       |       |                      |         |  |                          |         |  |                         |        |  |                    |         |  |                  |         |       |                |         |       |                 |         |       |               |         |       |                |       |    |               |         |    |  |
| Stripping Vapor  | 400.015             | mol/s |  |          |       |       |                      |         |  |                          |         |  |                         |        |  |                    |         |  |                  |         |       |                |         |       |                 |         |       |               |         |       |                |       |    |               |         |    |  |
| Rectify Vapor  | 400.006             | mol/s |  |          |       |       |                      |         |  |                          |         |  |                         |        |  |                    |         |  |                  |         |       |                |         |       |                 |         |       |               |         |       |                |       |    |               |         |    |  |
| Condenser Duty   | 15554               | kW    |  |          |       |       |                      |         |  |                          |         |  |                         |        |  |                    |         |  |                  |         |       |                |         |       |                 |         |       |               |         |       |                |       |    |               |         |    |  |
| Reboiler Duty  | 18417.6             | kW    |  |          |       |       |                      |         |  |                          |         |  |                         |        |  |                    |         |  |                  |         |       |                |         |       |                 |         |       |               |         |       |                |       |    |               |         |    |  |

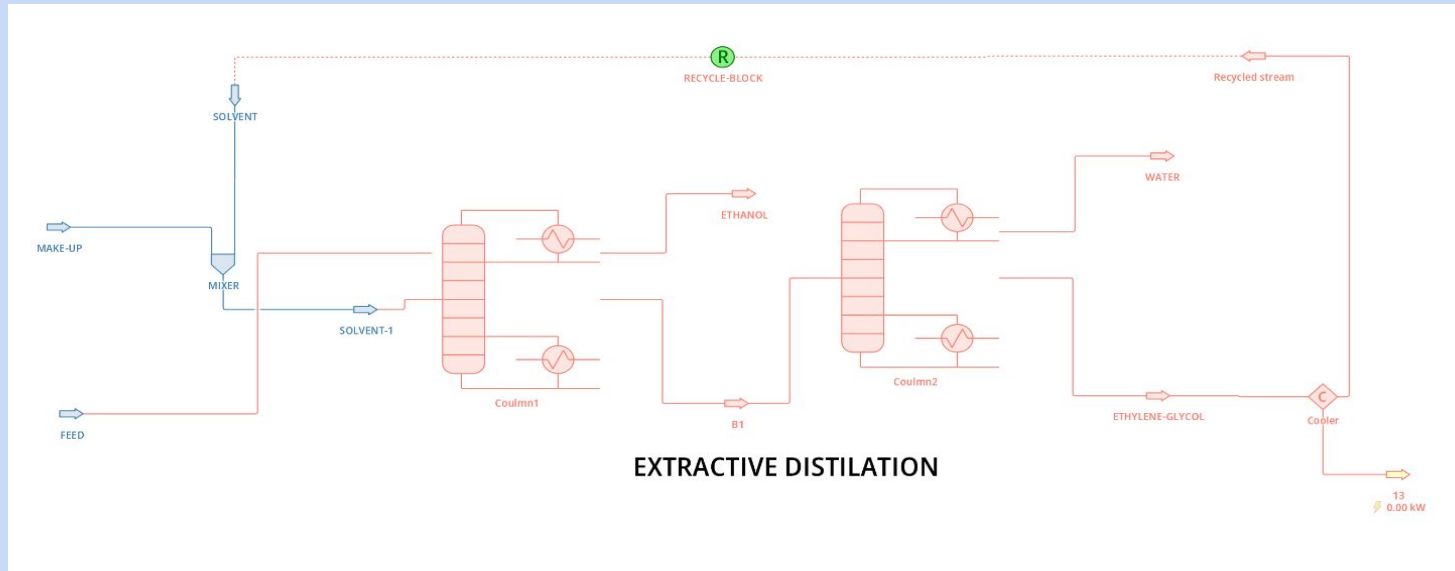


**Chem-sep Column Design**

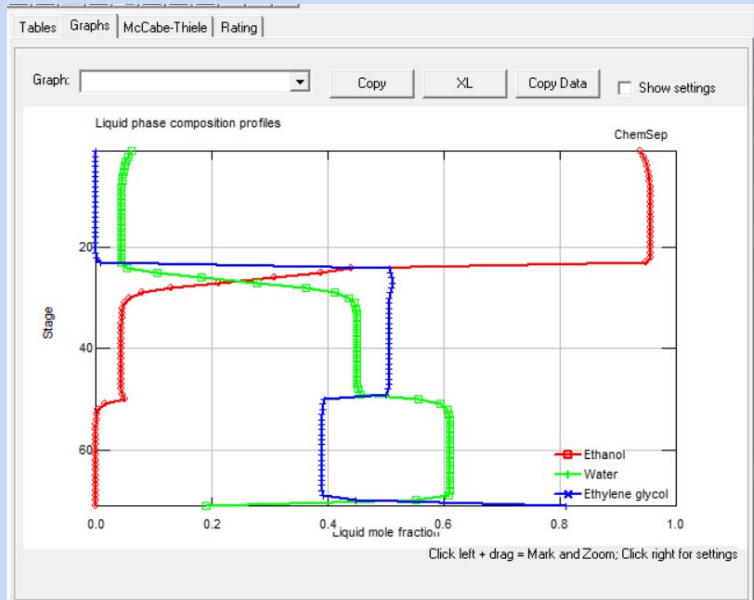
2. We did Separation of Azeotropic mixture by Extractive Distillation using DWSIM software for the system of ethanol and water.

## Extractive Distillation

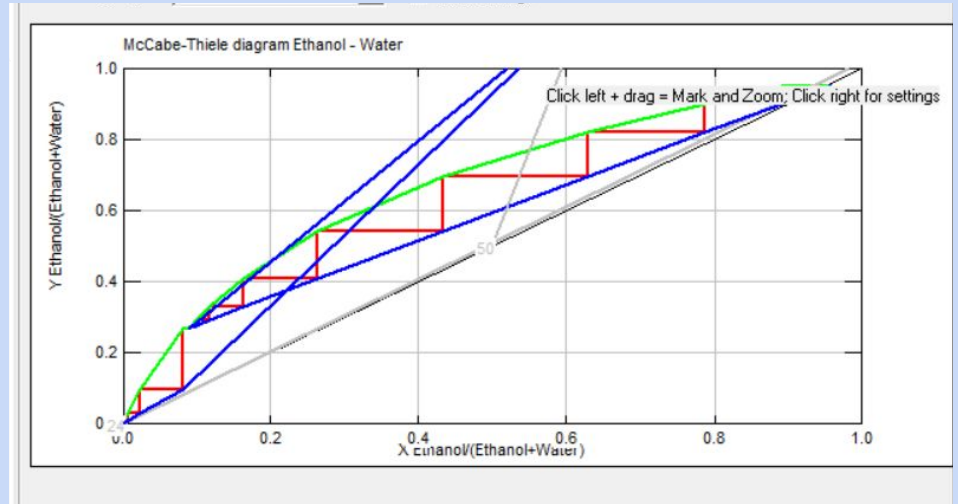
Extractive distillation separates a binary mixture by adding a third component. The third component is less volatile and doesn't evaporate during distillation. Or, raise the boiling point



# Composition of Ethanol, Ethylene Glycol & Water at each stage in Chem-Sep Column 1



# McCabe-Thiele Diagram (Column 1)



### **3.Performed Pressure Swing Distillation Through DWSIM Software.**

#### **Pressure Swing Distillation**

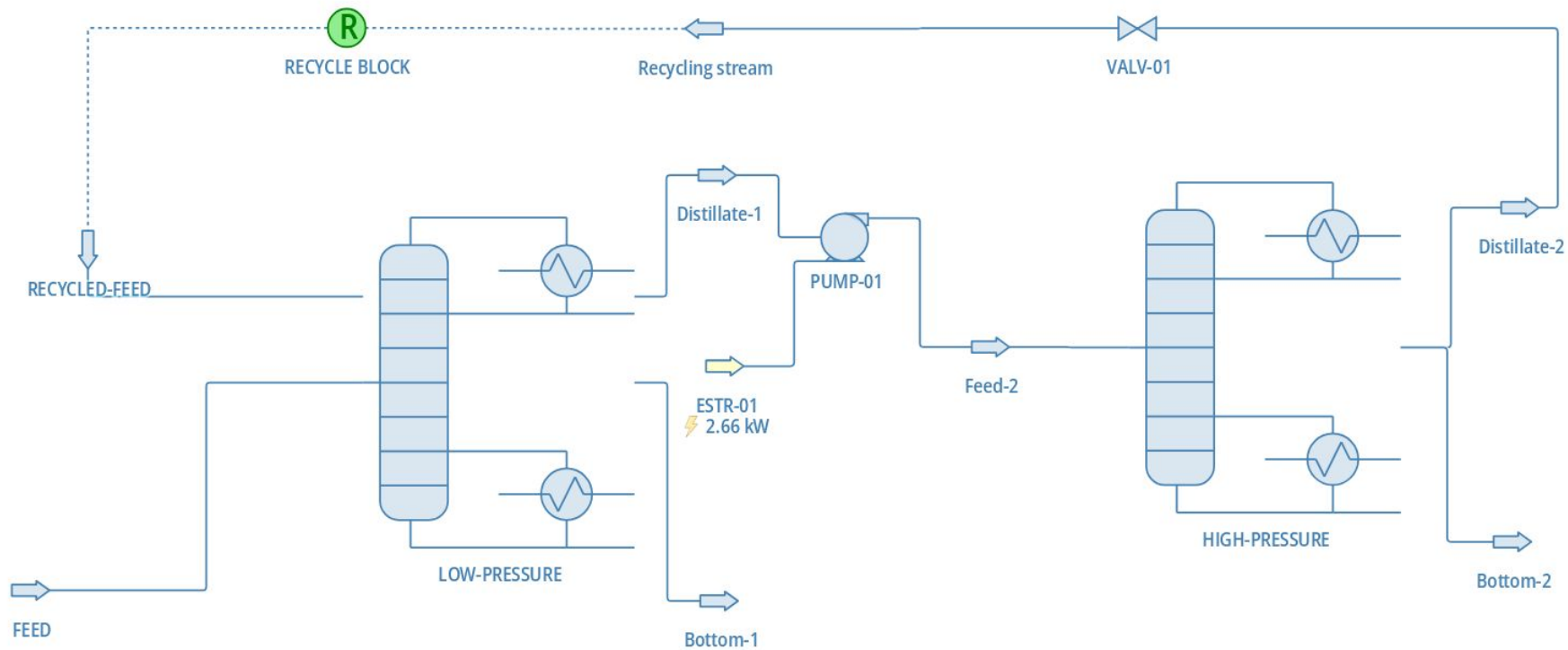
Process and chemical industries use pressure swing distillation to extract azeotropes. Azeotropes are liquid mixes that do not separate when boiling, meaning the gas and liquid phases are identical.

#### **Principle Of Pressure Swing Distillation**

At constant pressure, azeotrope mixes may contain more than one azeotropy point, but this is uncommon.

When pressure fluctuates, the azeotropy point moves. At different pressures, the same liquid combination forms a distinct azeotrope.

Since pressure can vary the relative volatility of a liquid combination, many azeotropes lose their azeotropy when the pressure is raised to a specific degree. A distillation column can separate the azeotropic system.

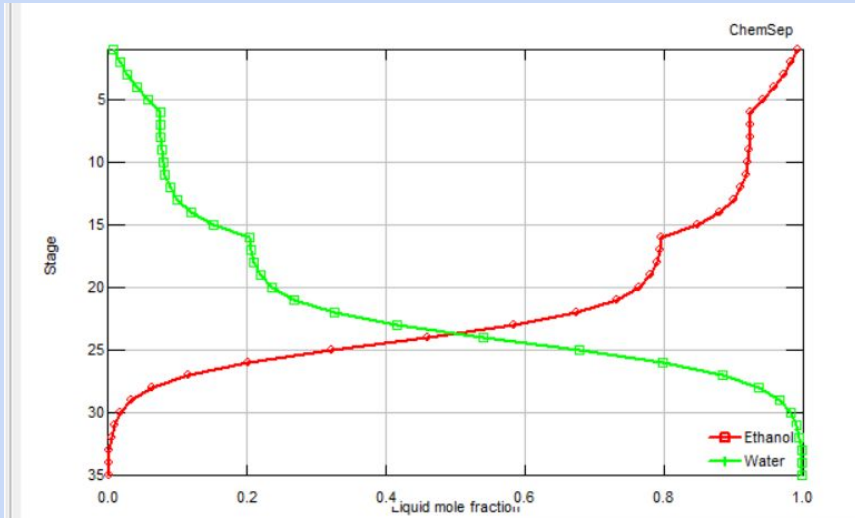


**Flow Sheet showing Pressure Swing Distillation**

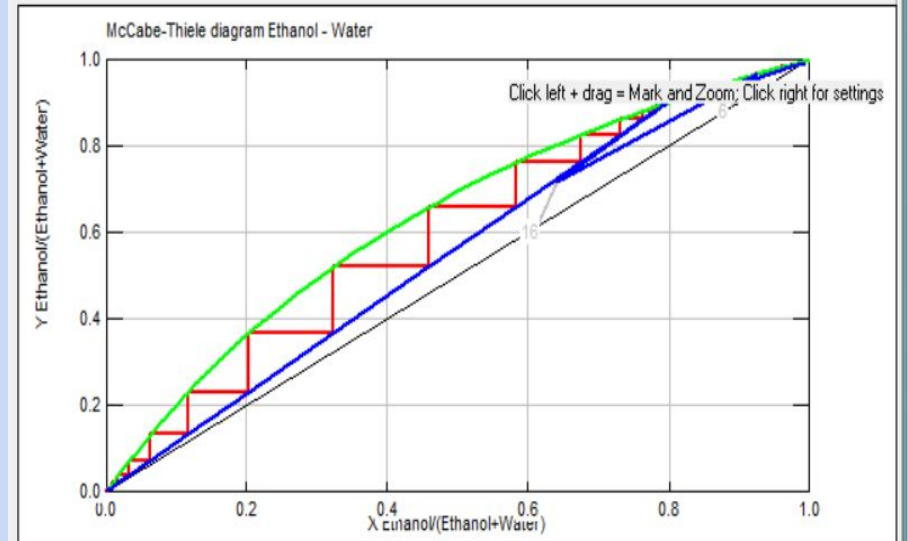


# Results from Low-Pressure Column

## Compositions of Ethanol and Water

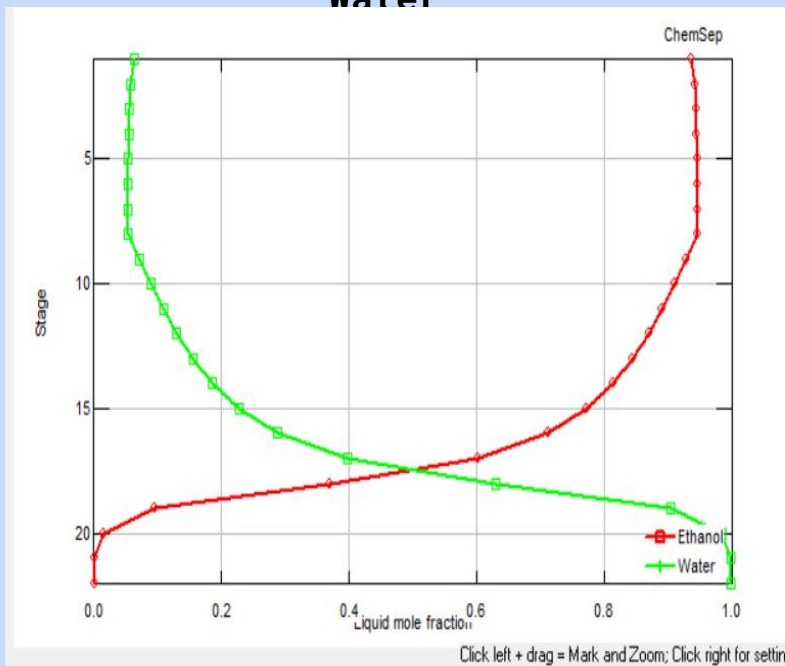


## McCabe thiele Diagram

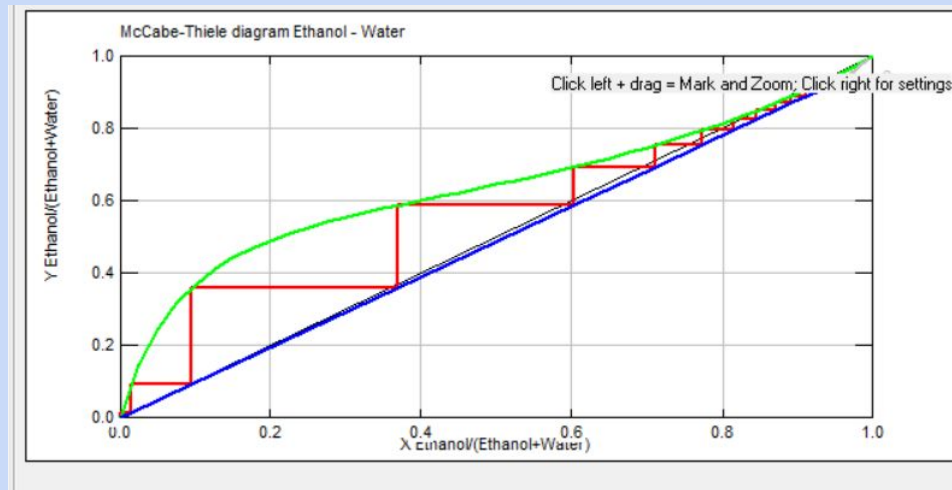


# Results from High-Pressure Column

## Composition Of Ethanol and Water



## McCabe-Thiele Diagram



**THANK YOU !!!**

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